# **Consequence Data**

The effects zone for each hazardous outcome is presented in terms of the maximum downwind extent. The consequence modelling results are presented in Table 8.8.1 to Table 8.8.4.

### Table 8.8.1 Sample Consequence Results for Biogas Facility

Comments.	Consequence Result (m)			
Scenario	Flame Length	LFL	Fireball Radius	
25mm Compressor Leak Booster	4	1	-	
25mm Compressor Leak Siloxane Removal	4	1	-	
25mm Vessel Leak Dehumidifier	4	1	-	
25mm Vessel Leak Digester	4	1	-	
25mm Vessel Leak Digester(E)	4	1	-	
25mm Vessel Leak Digester(W)	4	1	-	
25mm Vessel Leak Gas Holder (E)	4	1	-	
25mm Vessel Leak Biogas Holder	4	1	-	
25mm Vessel Leak H2S Removal	4	1	-	
500mm Vessel Leak Dehumidifier	50	28	-	
500mm Vessel Leak Digester(E)	51	32	-	
500mm Vessel Leak Digester(W)	50	29	-	
500mm Vessel Leak Gas Holder (E)	50	29	-	
500mm Vessel Leak Siloxane Removal	50	28	-	
500mm Vessel Rupture Biogas Holder	50	29	-	
500mm Vessel Rupture Booster	50	28	-	
500mm Vessel Rupture Digester	51	32	-	
500mm Vessel Rupture H2S Removal	50	28	-	
Catastrophic Rupture Digester(E)	-	24	25	
Catastrophic Rupture Digester(W)	-	24	29	
Catastrophic Rupture Gas Holder (E)	-	26	29	
Catastrophic Rupture Biogas Holder	-	31	38	
Catastrophic Rupture Dehumidifier	-	16	12	
Catastrophic Rupture Digester	-	30	35	
Catastrophic Rupture H2S Removal	-	16	12	
Catastrophic Rupture Siloxane Removal	-	14	10	

Note:

W: West Biogas System E: East Biogas System

## Upgrading of Tai Po Sewage Treatment Works

## Table 8.8.2 Sample Consequence Results for TPGPP

	Consequence Result (m)				
Scenario	Flame Length	Pool Radius	LFL	Fireball Radius	
10mm Leakage of Naphtha Importing and Tank Farm	15.8	-	18.8	-	
25mm Leakage of Naphtha Importing and Tank Farm	34.2	-	18.8	-	
75mm Leakage of Naphtha Importing and Tank Farm	85.8	38.9	18.8	-	
Full bore Rupture of Naphtha Importing and Tank Farm	62.1	38.9	18.8	-	
10mm Leakage of Naphtha Pumping and Distribution Headers to PTs	12.9	4.5	18.8	-	
25mm Leakage of Naphtha Pumping and Distribution Headers to PTs	27.7	14.4	18.8	-	
75mm Leakage of Naphtha Pumping and Distribution Headers to PTs	61.1	38.9	18.8	_	
Full bore Rupture of Naphtha Pumping and Distribution Headers to PTs	64.1	38.9	18.8	-	
10mm Leakage of Natural Gas Receiving Station and Distribution Headers to PTs	13.4	-	18.8	-	
25mm Leakage of Natural Gas Receiving Station and Distribution Headers to PTs	30.0	_	18.8	_	
75mm Leakage of Natural Gas Receiving Station and Distribution Headers to PTs	72.1	_	18.8	-	
Full bore Rupture of Natural Gas Receiving Station and Distribution Headers to PTs	160.4	_	18.8	-	
10mm Leakage of Phase II Production Units - PT5	8.0	-	18.8	-	
25mm Leakage of Phase II Production Units - PT5	18.2	-	18.8	-	
75mm Leakage of Phase II Production Units - PT5	46.8	-	18.8	-	
Full bore Rupture of Phase II Production Units - PT5	57.3	-	18.8	-	
Catastrophic Rupture of Phase II Production Units - PT5	-	-	18.8	23.1	
10mm Leakage of Phase I Production Units - PT2	8.0	-	18.8	-	
25mm Leakage of Phase I Production Units - PT2	18.2	-	18.8	-	

## Upgrading of Tai Po Sewage Treatment Works

	Consequence Result (m)				
Scenario	Flame Length	Pool Radius	LFL	<b>Fireball Radius</b>	
75mm Leakage of Phase I Production Units - PT2	46.8	-	18.8	-	
Full bore Rupture of Phase I Production Units - PT2	57.3	-	18.8	-	
Catastrophic Rupture of Phase I Production Units - PT2	-	-	18.8	23.1	
10mm Leakage of Phase I Production Units - PT3	8.0	-	18.8	-	
25mm Leakage of Phase I Production Units - PT3	18.2	-	18.8	-	
75mm Leakage of Phase I Production Units - PT3	46.8	-	18.8	-	
Full bore Rupture of Phase I Production Units - PT3	57.3	-	18.8	-	
Catastrophic Rupture of Phase I Production Units - PT3	-	-	18.8	23.1	
10mm Leakage of Phase I Production Units - PT4	8.0	-	18.8	-	
25mm Leakage of Phase I Production Units - PT4	18.2	-	18.8	-	
75mm Leakage of Phase I Production Units - PT4	46.8	-	18.8	-	
Full bore Rupture of Phase I Production Units - PT4	57.3	-	18.8	-	
Catastrophic Rupture of Phase I Production Units - PT4	-	-	18.8	23.1	
10mm Leakage of Phase II Production Units - PT5	8.0	-	18.8	-	
25mm Leakage of Phase II Production Units - PT5	18.2	-	18.8	-	
75mm Leakage of Phase II Production Units - PT5	46.8	-	18.8	-	
Full bore Rupture of Phase II Production Units - PT5	57.3	-	18.8	-	
Catastrophic Rupture of Phase II Production Units - PT5	-	-	18.8	23.1	
10mm Leakage of Phase II Production Units - PT6	8.0	-	18.8	-	
25mm Leakage of Phase II Production Units - PT6	18.2	-	18.8	-	
75mm Leakage of Phase II Production Units - PT6	46.8	-	18.8	-	
Full bore Rupture of Phase II Production Units - PT6	57.3	-	18.8	-	
Catastrophic Rupture of Phase II Production Units - PT6		-	18.8	23.1	
10mm Leakage of Phase II Production Units - PT7	8.0	-	18.8	-	
25mm Leakage of Phase II Production Units - PT7	18.2	-	18.8	-	
75mm Leakage of Phase II Production Units - PT7	46.8	-	18.8	-	

## Upgrading of Tai Po Sewage Treatment Works

Scenario	Consequence Result (m)				
	Flame Length	Pool Radius	LFL	Fireball Radius	
Full bore Rupture of Phase II Production Units - PT7	57.3	-	18.8	-	
Catastrophic Rupture of Phase II Production Units - PT7	-	-	18.8	23.1	
10mm Leakage of Phase II Production Units - PT8	8.0	-	18.8	-	
25mm Leakage of Phase II Production Units - PT8	18.2	-	18.8	-	
75mm Leakage of Phase II Production Units - PT8	46.8	-	18.8	-	
Full bore Rupture of Phase II Production Units - PT8	57.3	-	18.8	-	
Catastrophic Rupture of Phase II Production Units - PT8	-	-	18.8	23.1	
10mm Leakage of Towngas Export and Others	8.1	-	18.8	-	
25mm Leakage of Towngas Export and Others	17.9	-	18.8	-	
75mm Leakage of Towngas Export and Others	45.6	-	18.8	-	
Full bore Rupture of Towngas Export and Others	158.5	-	18.8	-	

## Table 8.8.3 Sample Consequence Results for LPG Storage Facility

Scenario	Consequence Result (m)				
	Flame Length	LFL	Fireball Radius	BLEVE (0.3 Bar)	
25mm Liquid Leak Filling Storage Tanker	32	59	-	-	
25mm Liquid Leak Flexible Hose	32	59	-	-	
25mm Liquid Leak Line to Vaporiser	32	59	-	-	
25mm Liquid Leak LPG Road Tanker	32	59	-	-	
25mm Liquid Leak Storage Vessel	32	59	-	-	
50mm Liquid Leak Road Tanker	58	136	-	-	
50mm Vapour Leak Road Tanker	22	15	-	-	
Fullbore Rupture Filling Storage Tanker	58	136	-	-	
Fullbore Rupture Flexible Hose	58	136	-	-	
Fullbore Rupture Line to Vaporiser	58	136	-	-	
Catastrophic Rupture LPG Road Tanker	-	226	58	-	
Catastrophic Rupture Storage Vessel	-	173	46	-	
Catastrophic Rupture Vaporiser	-	327	81	-	
BLEVE Road Tanker	-	-	-	62	

## Table 8.8.4 Sample Consequence Results for Linde HKO Limited

Scenario	Consequence Result (m)				
	Flame Length	LFL	<b>Fireball Radius</b>	BLEVE (0.3 Bar)	
25mm gas leak of Acetylene Cylinder	21	17	-	-	
25mm gas leak of Hydrogen Cylinder	40	35	-	-	
Catastrophic Rupture of Acetylene Cylinder	-	4	6	-	
Catastrophic Rupture of Hydrogen Cylinder	-	22	16	-	
Multiple BLEVE of Acetylene Tank	-	-	-	13	
Multiple BLEVE of Hydrogen Tank	-	-	-	26	
BLEVE of Oxygen Tank	-	-	-	96	
BLEVE of Nitrogen Tank	-	-	-	98	
BLEVE of Argon Tank	-	-	-	56	
BLEVE of Carbon Dioxide Tank	-	-	-	52	